

Article

A Preliminary Study on an Alternative Ship Propulsion System Fueled by Ammonia: Environmental and Economic Assessments

Kyunghwa Kim ^{1,2,*}, Gilltae Roh ¹, Wook Kim ^{2,*} and Kangwoo Chun ^{1,*}

¹ Future Technology Research Team, Korean Register (KR), Busan 46762, Korea; gtroh@krs.co.kr

² Department of Electrical Engineering, Pusan National University (PNU), Busan 46241, Korea

* Correspondence: kimkh@krs.co.kr (K.K.); kimwook@pusan.ac.kr (W.K.); kwchun@krs.co.kr (K.C.)

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Abstract: The shipping industry is becoming increasingly aware of its environmental responsibilities in the long-term. In 2018, the International Maritime Organization (IMO) pledged to reduce greenhouse gas (GHG) emissions by at least 50% by the year 2050 as compared with a baseline value from 2008. Ammonia has been regarded as one of the potential carbon-free fuels for ships based on these environmental issues. In this paper, we propose four propulsion systems for a 2500 Twenty-foot Equivalent Unit (TEU) container feeder ship. All of the proposed systems are fueled by ammonia; however, different power systems are used: main engine, generators, polymer electrolyte membrane fuel cell (PEMFC), and solid oxide fuel cell (SOFC). Further, these systems are compared to the conventional main engine propulsion system that is fueled by heavy fuel oil, with a focus on the economic and environmental perspectives. By comparing the conventional and proposed systems, it is shown that ammonia can be a carbon-free fuel for ships. Moreover, among the proposed systems, the SOFC power system is the most eco-friendly alternative (up to 92.1%), even though it requires a high lifecycle cost than the others. Although this study has some limitations and assumptions, the results indicate a meaningful approach toward solving GHG problems in the maritime industry.

Keywords: ammonia; hydrogen; fuel cell; electric propulsion system; greenhouse gas (GHG); zero-emission ship

1. Introduction

Beginning in 2020, all ships have to meet sulfur regulation for the limit of 0.5% m/m (mass by mass) in the fuel oil used onboard ships. Therefore, it is required to either use fuels with a maximum sulfur content of 0.5% (0.5%S) or use cheaper and conventional heavy fuel oil (HFO) with an exhaust gas cleaning system, called a scrubber. Moreover, the International Maritime Organization (IMO) agreed to an initial greenhouse gas (GHG) strategy that aimed to cut the total carbon dioxide (CO₂) emissions from ships by at least 50% from the levels in 2008 by 2050 and to phase out GHG emissions from international shipping as soon as possible in this century [1].

Therefore, carbon-free fuels (especially, hydrogen (H₂) and ammonia (NH₃)) appear to be the most promising solutions for the IMO's GHG reduction target by 2050. The International Transport Forum (ITF) [2] assumes that, in the case of 80% carbon factor reduction, hydrogen and ammonia will account for around 70% of the fuel market. A study by Nick Ash [3] concluded that green ammonia, which is produced while using renewable electricity not emitting greenhouse gases at any point in its product lifecycle, is a technically feasible solution for decarbonizing international shipping. Moreover, the results from Lewis, J. [4] suggest that H₂ and NH₃ are the most promising zero-carbon fuel options for decarbonizing in the transportation sector. In addition, a report by the International Energy Agency

(IEA) [5] estimates that H₂ and NH₃ have the potential to meet the environmental target in shipping, but their cost of production is high relative to oil-based fuels.

Table 1 shows the characteristics of hydrogen and ammonia as fuels when compared with HFO. Hydrogen is the most abundant element in the universe, but it is rarely found in its pure form. Although hydrogen can be obtained from various sources, such as biomass or electrolysis, it is currently mostly produced from natural gas [6]. Therefore, its key barriers are the high fuel price and limited availability for maritime operations. In addition, Table 1 shows that the liquefaction of hydrogen requires a very low temperature of -253°C , which brings the high cost of liquefying and storage system onboard. In this regard, NH₃ is being discussed as an alternative fuel due to its higher volumetric energy density and ease of handling.

Table 1. Fuel properties of heavy fuel oil (HFO), hydrogen, and ammonia.

Fuel Property	Unit	HFO	Compressed Hydrogen (350 bar)	Liquid Hydrogen	Liquid Ammonia	Reference
Low heating value	MJ/kg (kWh/kg)	40.2 (11.17)	120.00 (33.33)	120.00 (33.33)	18.6 (5.17)	[7–10]
Volumetric energy density	MJ/m ³ (kWh/m ³)	39,564–42,036 (10,990–11,677)	5040 (1400)	8500 (2361)	14,100 (3917)	[5,9,11]
Min. auto-ignition temperature	°C	250	500–577	500–577	650–657	[7,8,12]
Boiling temperature at 1atm	°C	N/A	N/A	−253	−33.4	[8,9]
Condensation pressure at 25 °C	atm	N/A	N/A	N/A	9.90	[8]
Hydrogen content	% by mass	N/A	100.0	100.0	17.8	[7,8]

The volumetric energy density of liquid ammonia is higher than that of liquid hydrogen, which is one of the attractions for fuel storage onboard, as shown in Table 1. Moreover, the storage requirements of ammonia are similar to those of propane, with ammonia in liquid form at room temperature (25°C) when pressurized to 9.9 atm or temperature of $−33.4^{\circ}\text{C}$ at atmospheric pressure [8]. The main benefits of using NH₃ as fuel when compared to H₂ are as follows.

- NH₃ is a cost-efficient alternative in terms of fuel price, and it has already existing infrastructure (approximately 10.6–30.2 times cheaper than H₂) [9].
- NH₃/s volumetric hydrogen content is significantly greater than that of H₂ (about 1.7 times more than liquid-H₂).
- Transportation and storage technologies for NH₃ already exist and they are available today (annually, more than 18 M t of NH₃ is traded internationally) [13].
- NH₃ has acute toxicity with strong smell and is easy to detect, and the safety measures are commonly practiced.
- A carbon capture system (CCS) from an NH₃ production plant is a feasible option [5].

In the marine industry, many studies have been performed on using ammonia as a fuel for zero-emission ships. Under some assumptions, ammonia is estimated to be more cost-effective than other alternative fuels. Ammonia is more economically beneficial than methanol or hydrogen, as explained by the Crown [14]. Furthermore, Lloyd's Register (LR) and University Maritime Advisory Services (UMAS) [15] suggest that ammonia is more competitive than hydrogen because of the lower costs that are associated with onboard storage. Nick Ash [3] and Niels de Vries [16] highlight that the ammonia-fueled engine is the most likely initial entry point for ammonia as a marine fuel and it will need to begin during the 2020s to follow the de-carbonization timetable.

Moreover, as part of the de-carbonizing technology, several R&D projects or consortiums have undertaken the use of ammonia as a marine fuel: ‘The Green Ammonia Consortium’ in Japan since 2017 [17], and ‘ZEEDS (Zero Emission Energy Distribution at Sea)’ project in Northern Europe since

2019 [18]. There is also a joint effort between a maritime company (MAN Energy Solutions) and a wind turbine manufacturer (Siemens Gamesa Renewable Energy) to supply clean ammonia as fuel for marine purposes [19].

Mostly, this ammonia can be used as fuel in an engine or fuel cell. Firstly, the ammonia can be used as engine fuel. In the case of the automotive industry, there are many demonstrations of ammonia-fueled engine as a range extender of the lithium batteries pack. Especially, the NH₃-fueled truck was developed in the USA. In 2007 [20], an automobile (AmVeh) was developed in South Korea in 2013 [21], and Toyota showcased the first ammonia fueled sports car in 2013 [22].

Additionally, in the marine industry, the main engine (M/E) or genset (generator engine combined with alternator) manufacturers have already started developing a new type of engine (or genset) while using ammonia fuel. In 2008, Caterpillar filed a patent (US Patent US20100019506A1) for an ammonia-fueled engine and ancillary systems [23]. Additionally, in 2018, Wärtsilä signed a memorandum of understanding with Finland's Lappeenranta University of Technology (LUT) and the Nebraska Public Power District (NPPD) for the study of the development of gensets based on ammonia fuel.

Further, in 2018, MAN announced that the first ammonia unit could be in operation in a short time based on their liquid propane gas (LPG) engine. MAN also planned to undertake a risk assessment on the use of ammonia as a gaseous fuel for propulsion [24]. Recently, Alfa Laval, which is one of the marine fuel system developers, announced that it is exploring the next generation of fuel gas supply systems to accommodate LPG and eventually ammonia for engines [25]. In 2019, the Japan Engine Corporation (J-ENG) announced the launch of a new R&D program in collaboration with the National Maritime Research Institute, focusing on engine development for the combustion of carbon-free fuels (e.g., hydrogen and ammonia) [26].

Secondly, ammonia can be used as fuel in a fuel cell system. Until now, most fuel cell-powered ships directly use hydrogen as the main fuel instead of ammonia. However, In January 2020, a new project (ShipFC) was launched to install the world's first ammonia-fueled fuel cell on an offshore vessel (Viking Energy) funding from the European Union (EU) [27]. On the other hand, for other industries, ammonia has been adopted as the main fuel for the fuel cell. For example, the ammonia-fed solid-oxide fuel cell (SOFC) is approaching commercial status, with major developments underway by IHI Corporation in Japan [28]. Project Alkammonia concluded its work on cracked-ammonia-fed alkaline fuel cells (AFC) in the EU. In addition, some research works [14,29] mentioned ammonia to be the main fuel for polymer electrolyte membrane fuel cells (PEMFCs) as a low-cost approach.

Moreover, one of the companies in Denmark (RenCat) is commercializing technology to generate low-cost, high-purity hydrogen from ammonia, for use in fuel cells by replacing the traditional ruthenium-based catalyst with an iron-nickel alloy [30]. One research center in Australia, the Commonwealth Scientific and Industrial Research Organization (CSIRO), has also developed a metal membrane for extracting pure hydrogen from ammonia [31].

Therefore, the ammonia-fueled power systems are expected to be more promising based on rapidly developed technologies. In this regard, this paper proposes possible power systems while using ammonia as fuel based on a target ship. The rest of this paper is structured, as follows: in Section 2, detailed explanations of a target ship and assumptions made in this study are presented. In Section 3, four proposed systems are described and fuel consumptions are calculated and compared with the conventional system for each method. In Section 4, the amount of GHG emissions for each case are compared. Additionally, Section 5 provides an economic study that is based on the lifetime of a ship. Lastly, the results are reviewed and conclusions are presented. The novelty of this paper is that a new preliminary study on ammonia-fueled propulsion systems, which are promising de-carbonization solutions in the marine industry, are investigated from the long-term perspective.

2. Target Ship

Within the global fleet, container ships accounted for the largest share (23%) of carbon dioxide (CO_2) emissions [32], and the small container feeder ship has the highest emission control area (ECA) share (65.1%) than other container ship sizes [33]. Therefore, the target ship is selected as the container feeder ship of length 195 m and capacity of 2500 Twenty-foot Equivalent Unit (TEU) (Figure 1); it operates short-distance voyages (usually 3–6 days/voyage). The ship is equipped with one main engine with a power output of 13,500 kW, and three gensets with power outputs of 1500 kW, each according to several references [34–36]. This conventional ship is equipped with a scrubber and a selective catalytic reduction (SCR) to meet the sulfur oxides (SO_x) and NO_x regulation (Tier 3). Table 2 provides the detailed specifications of the target ship.

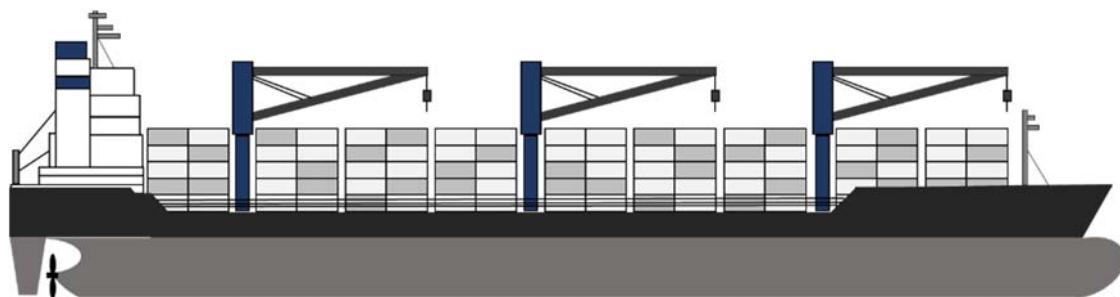


Figure 1. Typical layout of a 2500 (Twenty-foot Equivalent Unit) TEU container feeder ship.

Table 2. General specifications of the target ship.

Category	Specification
Length overall (LOA)	195 m
Breadth	32 m
Deadweight	30,000 t
Container capacity	2500 TEU (reefer: 500 TEU)
Ship speed	Max. 19.0 knots
M/E power output (MCR)	1 × 13,500 kW
Diesel gensets (MCR)	3 × 1500 kW
Fuel	HFO
Tank capacity	1800 m ³
Main voltage	AC 440V

Furthermore, for the target ship, the electric power demand is highly dependent on the reefer containers. In this study, it is assumed that the ship has 50% reefer containers (3.5 kW/reefer) onboard.

For a container feeder ship of this size, Table 3 illustrates a typical main engine load profile. In the Table, the time that is spent per year is based on reference [34], and the maneuvering time is given at the propulsion load of 5%. When maneuvering (or port in/out), the ship service load increased from 780 kW to 1800 kW, and it takes approximately 30 min. for each such operation. For this profile, the ship is at sea nearly 77% of the year (280 days) and in harbor operation for the remaining 23% (85 days).

Table 3. Assumed load profile and time spent in one year.

Propulsion Load Factor (%)	Propulsion Power (kW)	Electric Service Load (kW)	Reefer Container Load (kW)	Time Spent per Year (Hour)
100	13,500	780	875	336
85	11,475	780	875	2016
65	8775	780	875	3024
50	6750	780	875	336
35	4725	780	875	336
25	3375	780	875	336
10	1350	780	875	236
5	675	1800	875	100
0	-	550	875	2040

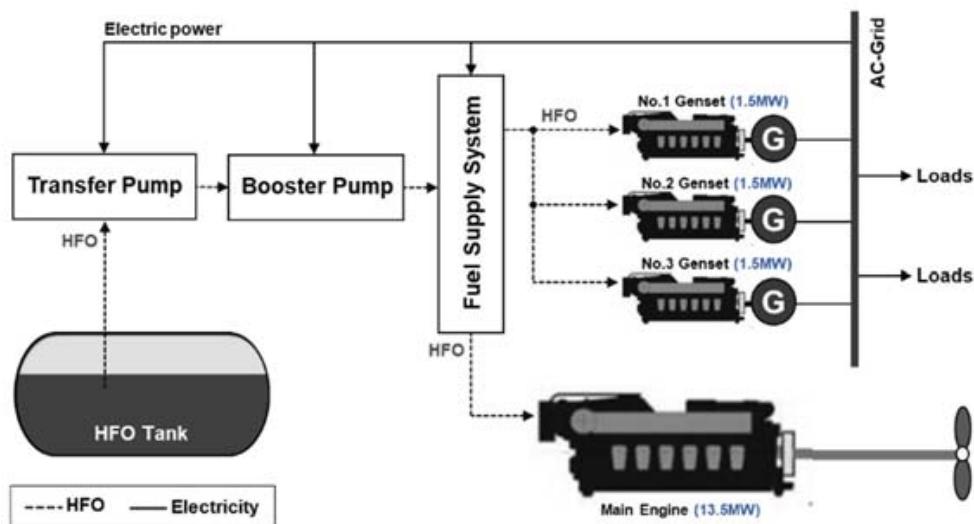
3. Proposed Systems

3.1. Description of Proposed Systems

In this study, the conventional power system using HFO fuel is referred to as Case 1, and four new propulsion systems (Cases 2–5) are suggested while using NH₃ fuel, as given below.

- Case 1. The conventional HFO-based M/E propulsion system.
- Case 2. The proposed NH₃-based M/E propulsion system.
- Case 3. The proposed NH₃-based electric propulsion system powered by generators.
- Case 4. The proposed NH₃-based electric propulsion system powered by PEMFC.
- Case 5. The proposed NH₃-based electric propulsion system powered by SOFC.

For Case 2, the propulsion configuration is the same as Case 1, except for the fuel type. For Case 3, the generators supply electric power to both the ship service load and propulsion load. For Cases 4 and 5, the generators are replaced with PEMFC and SOFC, respectively. Figures 2–6 show the concept system for each case.

**Figure 2.** The simplified concept system for Case 1.

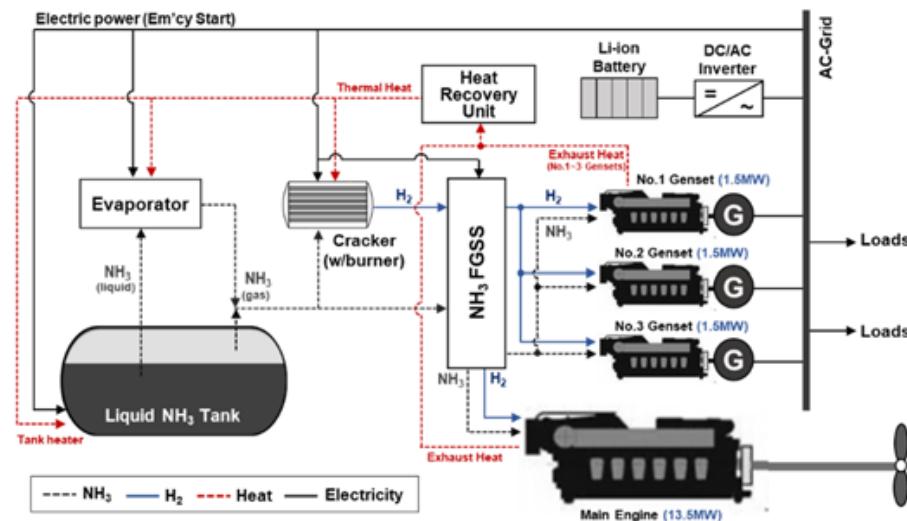


Figure 3. The simplified concept system for Case 2.

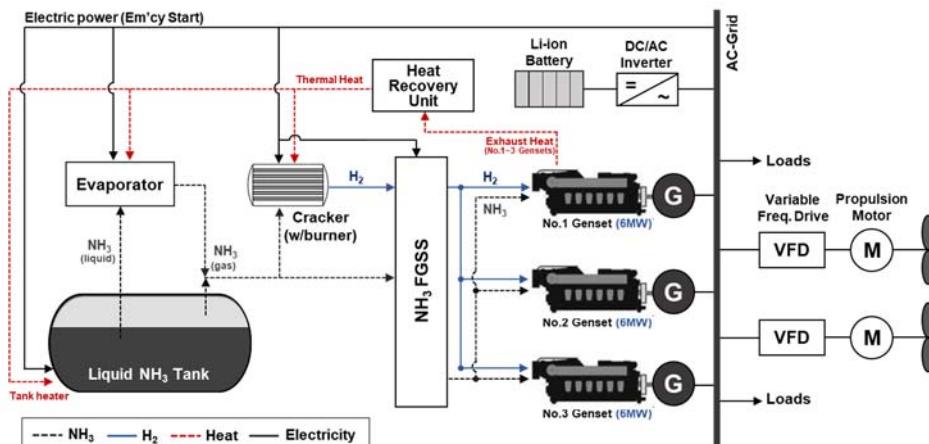


Figure 4. The simplified concept system for Case 3.

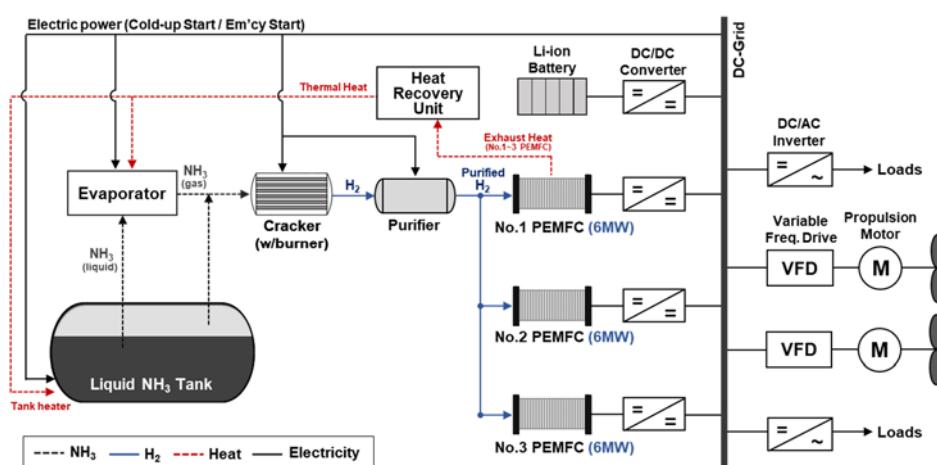


Figure 5. The simplified concept system for Case 4.

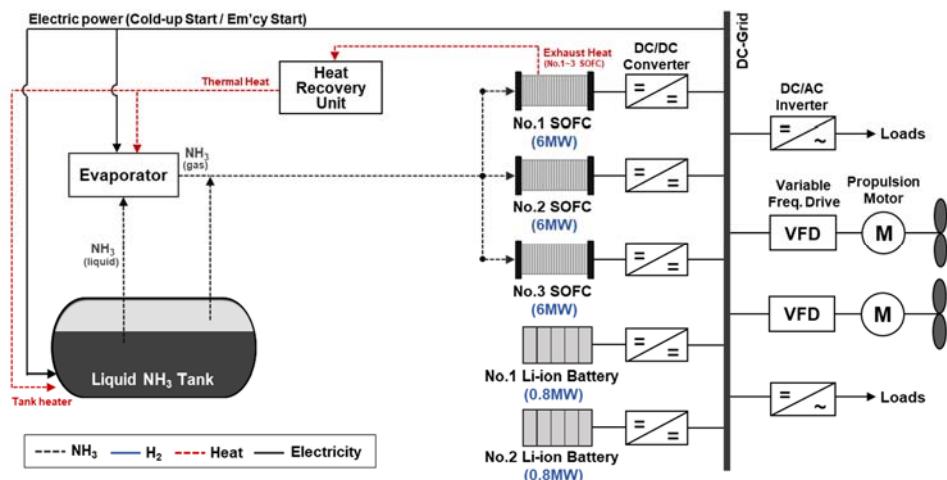


Figure 6. The simplified concept system for Case 5.

3.2. Main Equipment & System

3.2.1. Ammonia Engine

It is clear that pure ammonia shows low specific energy, high auto-ignition temperature, and it has narrow flammability limits (15–28% by volume in air), as shown in Table 1. This means that the combustion conditions are unstable at very low and very high engine speeds [3,7]. Consequently, hydrogen has been applied as a promoter for ammonia engines in many studies. M. Comotti et al. [37] successfully developed a cracking reactor housing for hydrogen generation and coupled it to an internal combustion engine that was fueled with ammonia. Frigo S. et al. [38] selected hydrogen as an engine combustion promoter and obtained it by reforming ammonia. In a study by C. S. Mørch et al. [39], the use of ammonia/hydrogen mixtures as an engine fuel was investigated in a series of experiments.

Hydrogen displays the lowest ignition energy, highest combustion velocity, and widest flammability range that allows for the engine to operate with very high air-fuel ratios. Therefore, a small amount of it, added to the air-ammonia mixture, is effective in speeding up combustion [40]. Of course, there are NH₃-fed engines that applied gasoline fuel as a support fuel. However, the best and carbon-free promoter is regarded as hydrogen.

Ammonia-hydrogen mixtures can be used in a compression ignition (CI) or a spark ignition (SI) internal combustion engine. The CI is bound to certain mixtures and their corresponding timings based on the principle of design. Furthermore, to use both fuels efficiently, the CI has a trade-off between high compression ratio to promote ammonia combustion and limited compression ratio to prevent hydrogen from ringing [41].

In this regard, some research works that were undertaken on the use of ammonia have been on spark ignition engines Niels de Vries [14] mentioned that using an SI engine instead of a CI engine results in a further reduction in harmful emissions. In addition, C. S. Mørch investigated the use of ammonia/hydrogen mixtures as an SI-engine fuel [39], by varying the excess air ratio and the ammonia to hydrogen ratio. Moreover, the study by Frigo S. et al. [42] aimed at determining the proper air-ammonia-hydrogen mixture composition for the actual operating conditions of a twin-cylinder 505 cm³ SI engine. Besides, C. Duynslaeger [43] examined the combustion characteristics of premixed ammonia-air mixtures under the elevated pressure and temperature conditions that were encountered in SI engine operations.

In another study, Valera-Medina [7] reviewed an SI engine that was fueled by ammonia and mentioned that ammonia is required to be vaporized with at least 4–5% (by weight) hydrogen for good performance. In other words, mixtures of approximately 30% hydrogen and 70% ammonia (by volume) have been reported. In this study, the mixture ratio between NH₃ and H₂ for spark ignition is assumed

based on references [3,14] and is given in Table 4. However, a separate fuel tank for hydrogen might not be a necessity because an onboard reformer could be used to crack a proportion of the ammonia into hydrogen (and nitrogen) to support combustion [3]. The cracking process itself is relatively simple, but further research is required to calibrate the rate of hydrogen cracking to support stable combustion conditions at variable engine loads and speeds.

Table 4. Assumed ammonia–hydrogen mixture for spark ignition (SI) engine.

Fuel	Energy Density	Weight Ratio	Energy Ratio
NH ₃	18.6 MJ/kg (5.17 kWh/kg)	95%	74.7%
H ₂	120.0 MJ/kg (33.33 kWh/kg)	5%	25.3%

3.2.2. PEMFC

The PEMFC is the most commercialized fuel cell type, and many fuel-cell-driven ships have already applied this type. The PEMFC is required to supply high purity hydrogen while using a purifier, which consumes approximately 2% [14] of the PEMFC's capacity to maintain proper flow and pressure. The other auxiliary equipment for operating the PEMFC systems (cracker, cooling, air supply fan, fuel supply pump, etc.) is assumed to be similar to the amount of auxiliary equipment load that is required for the conventional engine.

3.2.3. SOFC

The SOFC has a huge advantage, in that it can directly use NH₃ as fuel; however, the SOFC is limited in how rapidly it can increase fuel delivery rate according to power demand [44]. Therefore, the energy storage system (ESS) is utilized as a complement (back-up) power to compensate for the slow dynamics of the SOFC during transient operations, and it can also be used as a cold-start energy source. In other words, the ESS is charged through the remaining power at an instantaneous load reduction and it discharges at an instantaneous load increase. The ESS can cope with the extra load fluctuations, especially for high load conditions (ex. heavy weather, etc.).

3.2.4. ESS

For Cases 2, 3, and 4, at the cold start-up condition, the ammonia engine or fuel cell requires energy for ammonia cracking as well as vaporizing, and this could be supplied as electrical energy. In other words, during cold start-up, the cracker, evaporizer, and tank heater are electrically heated [42], and the amount of energy is assumed to be approximately 10 Wh (per kW of engine capacity) [37]. On the other hand, in the case of the PEMFC, it is assumed to be about 19 Wh (per kW of PEMFC capacity) based on a reference [45].

For Case 5, which directly uses ammonia, the ESS could be used for maneuvering power at port-in/out due to the slow dynamics of the SOFC. The additional increased load for the port-in/out is 1020 kWh; therefore, the ESS capacity that is demanded (E_{demand}) for Case 5 is at least over 1020 kWh. Based on the E_{demand} , the installed ESS capacity ($E_{installed}$) is calculated, as below (Equation (1)), which is modified to a simple expression based on a reference [46]. In this study, it is assumed that DoD (k_{dod}) is 80%, total system efficiency (k_e) is 96%, and safety margin (k_a) is 20% while considering battery aging (degradation) during its lifetime.

$$E_{installed} \geq \frac{E_{demand}}{k_{dod} \times k_e} \times (1 + k_a) \text{ [kWh]} \quad (1)$$

Therefore, the $E_{installed}$ are selected as 300 kWh for Cases 2 and 3550 kWh for Case 4, and ESS of 1600 kWh for Case 5.

3.2.5. Cracking

Ammonia can be dissociated (or cracked) into nitrogen and hydrogen via the reaction [47]:



Ammonia cracking is an endothermic reaction that requires a heat source (46.22 kJ/mol) [48] that is capable of maintaining the catalyst at the proper cracking temperature and, thus, delivering the required reaction enthalpy. Further, the dissociation rate depends on the temperature, pressure, and catalyst type [37]. The theoretical adiabatic efficiency for the thermocatalytic reaction is approximately 85% relative to the energy of the released hydrogen. Additionally, additional energy would be required to overcome thermal losses in the cracking process [48]. In this study, it is assumed that the cracker efficiency is about 80% based on several references [49,50].

In addition, for Cases 2 and 3, as per references [14,48], the exhaust gases and the cooling system from the engine can be utilized to supply heat to the cracker, evaporator, and the tank heater [14]. In other words, this recycled heat would be sufficient, because it only required a small percentage of H₂ as a pilot fuel. For Case 4, the PEMFC operates with high-temperature conditions, and the heat could be utilized to supply heat to both the evaporator and the tank heater [14].

3.2.6. BOG and Vaporizing

Today, the Haber–Bosch process produces most ammonia on a large scale by and the generated liquid ammonia from the process is stored in tanks. A portion of the ammonia continuously evaporates, creating a gas called boil-off gas (BOG), due to heat entering the tanks during storage. The BOG leads to an increase in the pressure in tanks and loss of ammonia through the safety (or blow-off) valve, which could cause economic and safety problems. Therefore, similar to LNG carriers, this BOG could be reused as power sources.

Equation (3) could be applied to determine the BOG of the liquid ammonia inside a tank [51].

$$\text{BOG} = \frac{\text{NH}_{3,\text{Evap}}}{\text{NH}_{3,\text{Storage}}} \times 100\% = \frac{U \times A \times \Delta T}{\text{NH}_{3,\text{Storage}} \times \Delta H_{\text{Vap}}} \times 100\% \quad (3)$$

where NH_{3,Evap} is the mass of evaporated ammonia produced in a single day and NH_{3,Storage} is the amount of available storage. ΔH_{Vap} [kJ/kg] is the heat of vaporization for liquid ammonia at -33 °C and U [W/(m²·K)] is the overall heat transfer coefficient for the tank, and ΔT is the temperature difference between the tank and outside air. A [m²] is the surface area of a tank. Typically, the boil-off rate of ammonia fuel is around 0.04%/d or lower [51], which is a significantly lower value than LNG fuel due to the small temperature difference (ΔT).

3.3. Fuel Consumption

In general, the specific fuel consumption (SFC) is calculated, as below, based on the energy density of the fuel and the total system efficiency [52].

$$SFC_k(i) = \frac{1}{\delta(k) \times \eta} [\text{g/kWh}] \quad (4)$$

where *i* = the load factor of the M/E, genset or fuel cell. δ = the energy density of the fuel used [kWh/g] (Table 1). *k* = the fuel type (HFO, NH₃, H₂). η = the total system efficiency (Table 5).

However, the optimal load range of an engine lies between 70–85% [53]. Especially, in light load conditions, the engine runs less efficiently, and this phenomenon leads to a relative fuel increase when compared to the optimal operating conditions. In other words, the SFC of the fuel is different, depending on the load factor, and the modified SFC (SFC') is calculated, as below (Equation (5)). In

this study, the correction factors (L_f) according to different load factors are assumed in Table 6 based on references [54–57], and these may differ by manufacturers' specifications.

$$SFC'_k(i) = \frac{1}{\delta(k) \times \eta} \times L_f(i) [\text{g/kWh}] \quad (5)$$

Table 5 shows the system efficiency for each case based on references. For all cases, the total fuel consumption is the sum of the fuel demand for propulsion load (P_p) and ship service load (P_s), as below (Equation (6)). While using the SFC' , the total fuel consumption for one year (F_{total}) is calculated by adding the fuel used at each operating load time.

$$F_{total} = \sum_i \{P_p(i) \times T(i) \times SFC'_k(i)\} + \sum_i \{P_s(i) \times T(i) \times SFC'_k(i)\} [\text{g}] \quad (6)$$

where i = the load factor of the M/E, genset or fuel cell. k = the fuel type (HFO, NH₃, H₂). $P(i)$ = the power demand for the load factor (i) [kW]. $T(i)$ = the time spent for the load factor (i) [hours].

Table 5. The system efficiency (η) according to each case.

Case 1 & 2			Case 3			Case 4			Case 5		
Equipment	η (%)	Ref.									
M/E	0.52	[52,58]	Genset	0.50	[59]	Cracker	0.80	[49,50]	SOFC	0.65	[60]
Shafting	0.99	[58]	Alternator	0.98	[58]	H ₂ purifier	0.90	[50]	Converter	0.98	[61,62]
Genset	0.50	[59]	Switchboard	0.98	[63]	PEMFC ²	0.65	[55,56]	Switchboard	0.98	[63]
Alternator	0.98	[58]	VFD ¹	0.97	[64,65]	Converter	0.98	[61,62]	Inverter	0.98	[66]
Switchboard	0.98	[63]	Prop. motor	0.98	[58]	Switchboard	0.98	[63]	VFD ¹	0.97	[64,65]
-	-	-	-	-	-	Inverter	0.98	[66]	Prop. motor	0.98	[58]
-	-	-	-	-	-	VFD ¹	0.97	[64,65]	-	-	-
-	-	-	-	-	-	Prop. motor	0.98	[58]	-	-	-
η_{prop} ³	0.51	-	η_{prop} ³	0.46	-	η_{prop} ³	0.43	-	η_{prop} ³	0.59	-
$\eta_{service}$ ⁴	0.48	-	$\eta_{service}$ ⁴	0.48	-	$\eta_{service}$ ⁴	0.44	-	$\eta_{service}$ ⁴	0.61	-

¹ VFD: Variable Frequency Drive (also known as motor drive). ² The average value of the peak efficiency on the references. FCM 120 model is applied in the case of reference [56]. ³ The total efficiency of the propulsion system.

⁴ The total efficiency of the ship service power system.

Table 6. Assumed correction factors (L_f) according to different load factors.

Load Factor (i) (%)	Main Engine/Genset	PEMFC	SOFC
85 < i ≤ 100	1.02	1.25	1.14
65 < i ≤ 85	1.00	1.19	1.09
50 < i ≤ 65	1.01	1.12	1.06
35 < i ≤ 50	1.04	1.07	1.04
25 < i ≤ 35	1.09	1.03	1.00
10 < i ≤ 25	1.13	1.00	1.06
i ≤ 10	1.21	1.67	1.43

For Cases 1 and 5, which are fueled by HFO and NH₃, respectively, the fuel consumption is just calculated while using Equation (6). However, for Cases 2 and 3, the total fuel consumption is calculated by summing the amount of NH₃ for direct use and the amount of NH₃ for cracking by using Table 4. Additionally, the hydrogen content of ammonia is 17.8%/mass (Table 1), which means that the NH₃ for cracking is required about 6.18 times (including 10% loss) more than direct use to produce

hydrogen. Furthermore, for Case 4, the fuel consumption is dependent on the PEMFC, which is only fueled by hydrogen from the NH_3 cracking process.

Additionally, in Case 1, it is assumed that the scrubber requires 20 kW additional power per MW engine output [67] and, in Case 5, the additional power is required at harbor mode ($i = 0\%$) for ESS charging. For Cases 1, 2, and 3, which have installed SCR, it is assumed that additional fuel (8%) is required for operating the SCR at the port in/out and at harbor [68].

Moreover, for Cases 2 to 5, while considering the naturally generated BOG in the storage tank (F_{BOG}), the fuel demand for one year (F_{demand}) is calculated, as below. In Equation (7), the boil-off rate (r) is assumed as 0.04% [51], and the efficiency of the BOG return system (η_B) is assumed as 80%.

$$F_{demand} = F_{total} - F_{BOG} = \left(1 - \frac{r \times 365}{100} \times \eta_B\right) \times F_{total} [\text{g}] \quad (7)$$

Table 7 shows the results of the total fuel consumption for each case. Case 4, which is powered by hydrogen-based PEMFC, has the highest fuel consumption, despite the hydrogen's high energy density, which is generated from ammonia cracking. Case 5, which is powered by ammonia-based SOFC, has the lowest fuel consumption, due to its high energy efficiency and its non-cracking system.

Table 7. Total weight and volume of fuel consumption for each case.

Item	Case 1 (HFO)	Case 2 (NH_3)	Case 3 (NH_3)	Case 4 (NH_3)	Case 5 (NH_3)
Total weight of fuel consumption (t/y)	13,507.0 (1.00 base)	25,505.7 (1.89 times)	28,083.4 (2.08 times)	33,889.0 (2.51 times)	22,447.3 (1.66 times)
Total volume of fuel consumption (m^3/y)	14,289.0 (1.00 base)	33,645.8 (2.35 times)	37,046.1 (2.59 times)	44,704.6 (3.13 times)	29,611.4 (2.07 times)

3.4. Volume and Weight

Ammonia has lower volumetric energy density and low heating value (LHV) than the conventional HFO fuel. Therefore, if a ship applied the proposed systems, it takes cargo loss inevitably, due to the decreasing space and dead weight tonnage (DWT) due to the ammonia fuel storage. In this study, Table 8 shows the assumed volume and weight for each piece of equipment.

Table 8. Assumed volume and weight for each equipment.

Equipment	Capacity	Volume (m^3)	Weight (t)	Reference
Main Engine	13.5 MW	370.7	394.0	[69]
Genset	1.5 MW	35.9	20.8	[59]
	6.0 MW	145.3	115.0	[59]
PEMFC ¹	6.0 MW	50.9 ²	19.5	[70,71]
SOFC ¹	6.0 MW	874.9 ²	271.5	[60,72,73]
ESS ³	300 kWh	4.2	4.0	[74]
	550 kWh	7.7	7.4	[74]
	1600 kWh	33.3 ²	21.4	[74]
Cracker ⁴ (Case 2,3)	-	6.3	3.0	[75]
Cracker ⁴ (Case 4)	-	19.5	8.0	[75]
DC/AC converter	300 kW	2.7	1.1	[76]
DC/DC converter (ESS)	600 kW	4.0	1.8	[76]
	1600 kW	10.7	4.8	[62]

Table 8. Cont.

Equipment	Capacity	Volume (m ³)	Weight (t)	Reference
DC/DC converter (F/C)	6.0 MW	30.6	14.0	[77]
VFD	7.0 MW	30.9	8.0	[78]
Propulsion Motor	6.7 MW	28.0	17.8	[79]
SCR ⁵	18 MW	90.0	17.0	[80]
Scrubber	18 MW	150.0	33.0	[80]

¹ Assumed value based on references. Excluding auxiliary equipment (balance of plant) from the package system.

² Assumed value based on references. A space margin of 50% is included for the separation distance between each pack, in view of the possibilities of an optimal layout design for large scale applications. This can be changeable depending on the safety requirements and location environment. ³ Excluding the inverter/converter. ⁴ Assumed value based on reference due to the lack of suitable manufacturer's data for the capacity. ⁵ Including reactor and catalyst.

Figure 7; Figure 8, while using Table 7, compare the results of total volume and weight for each case. In case of the weight, it is assumed that there is only half the amount of fuel in a fuel tank. In each case, the ratio of the main equipment was different. Among the cases, Case 5 required the largest volume and weight, owing to the high percentage of SOFC. In particular, the effect of volume increase is greater than weight, which is equivalent to cargo losses of about 87 TEU 20ft containers [81,82] as compared to Case 1. Therefore, alternative technologies (lightweight hull materials, optimized space layout, etc.) need to be considered to compensate for this.

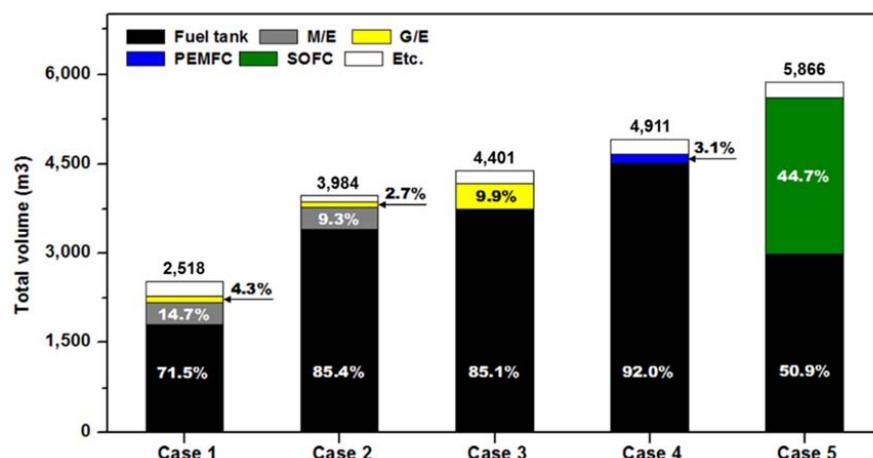


Figure 7. Total volume comparison of each case.

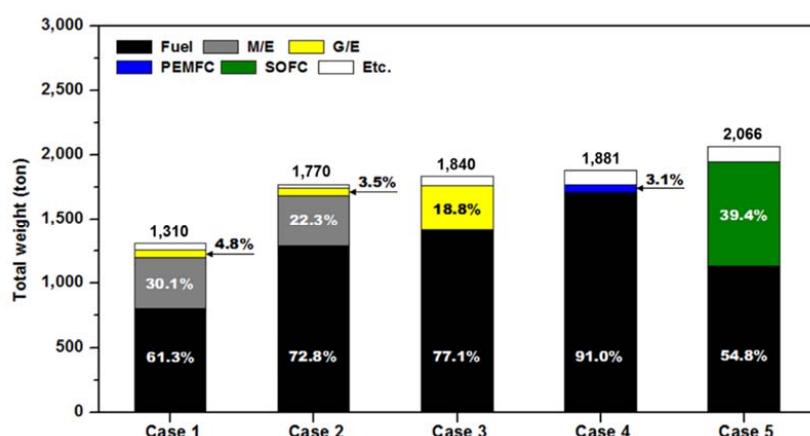


Figure 8. Total weight comparison of each case.

4. Environmental Analysis

The environmental impacts are compared for each case being focused on GHG emissions. The other types of emissions (SO_x , NO_x , and particulate matter (PM)) are not necessary for comparison due to the installation of SCR and scrubber for Case 1. In the case of ammonia fuel, the Haber–Bosch process can produce it in great quantities from natural gas, which is not an eco-friendly solution due to the steam methane reformation (SMR) emissions for hydrogen production. Therefore, the SMR is mostly integrated with carbon capture and storage (CCS). However, ammonia could also be produced by renewable or waste energy though the water electrolysis process. Therefore, the emission factor of NH_3 is divided into two: the SMR with CCS method and the electrolysis method. Table 9 shows the emission factors for each fuel type [10,83].

Table 9. Greenhouse gas (GHG) emission factors for each fuel type.

Fuel	$\text{CO}_2 \text{ t/t Fuel}$		$\text{CH}_4 \text{ t/t Fuel}$		$\text{N}_2\text{O} \text{ t/t Fuel}$	
	Upstream	Operation	Upstream	Operation	Upstream	Operation
HFO	0.338	3.114	0.0032	0.0001	-	0.00016
NH_3 (SMR+CCS)	0.231	-	-	-	0.00001	-
NH_3 (electrolysis)	0.168	-	-	-	0.00001	-

Additionally, the total life cycle emissions are both upstream emissions and operational emissions. The upstream emissions are the emissions generated from the fuel production and transportation processes, whereas the operational emissions are the emissions that are generated from the ship's operation.

GHG emissions are calculated while using the CO_2 -equivalent global warming potential by directly summing the 100-year conversion coefficients recommended by the 5th assessment report (AR5) of the Intergovernmental Panel for Climate Change (IPCC) for the three main GHG emission types (CO_2 , CH_4 , and N_2O) [84]. Therefore, the GHG emission factors ($E_f(\text{GHG})$) are calculated as:

$$E_f(\text{GHG}) = E_f(\text{CO}_2) + 28 \times E_f(\text{CH}_4) + 265 \times E_f(\text{N}_2\text{O}) [\text{t}\cdot\text{CO}_2^{-e}/\text{t}\cdot\text{fuel}] \quad (8)$$

As shown in Figure 9; Figure 10, among all of the cases, Case 5 is the most eco-friendly system that requires the lowest fuel consumption. When comparing with Case 1, Case 5 could reduce GHG emissions by approximately 89.2% (SMR with CCS) or 92.1% (electrolysis). For all cases, the ammonia fuel by electrolysis would be more environmentally beneficial than SMR with the CCS method. The upstream emissions are given a higher impact when it comes to the ammonia fuel; however, the operational emissions have a significant effect on the HFO. Therefore, it is noted that CO_2 -neutral shipping seems to be possible for ammonia-fueled ships.

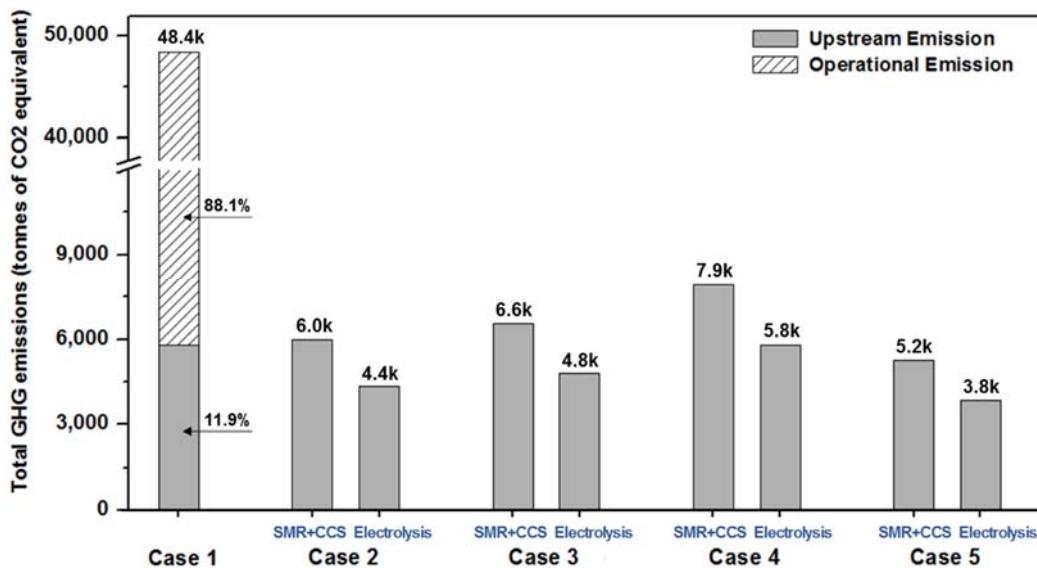


Figure 9. Total GHG emissions for each case focused on upstream and operational emissions.

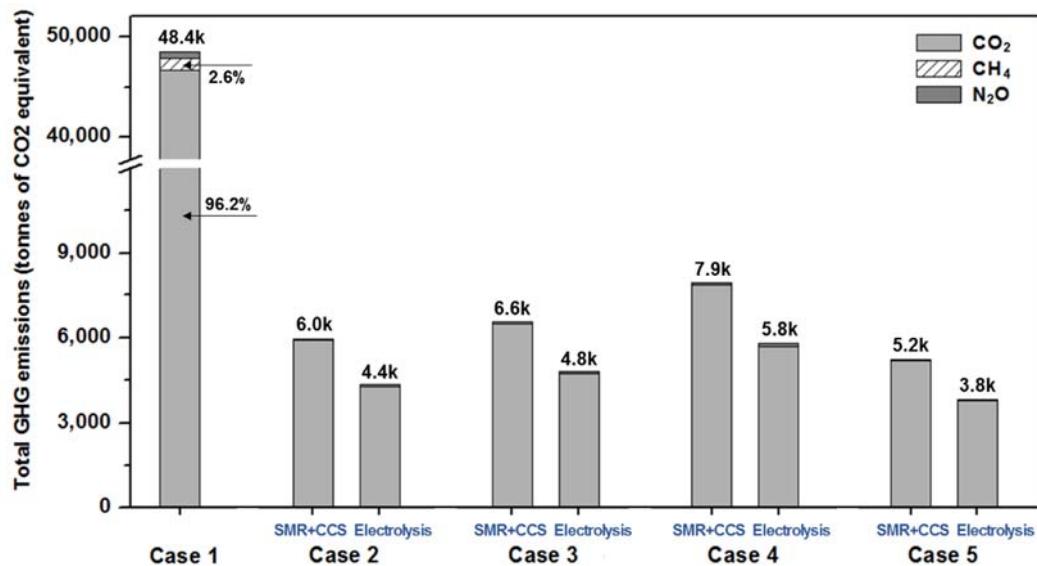


Figure 10. Total GHG emissions for each case focused on main emission types.

5. Economic Analysis

The cumulative cost for the lifespan of a ship is calculated, as below, based on a reference [85] while using the capital expenditure (CAPEX) and the operating expense (OPEX).

$$\text{Cumulative cost} = \text{CAPEX} + \sum_{n=1}^{n=25} \frac{\text{OPEX} \times (1+i)^n}{(1+r)^n} \quad (9)$$

where n is the age of ship from 1 to 25 years, r is the discount rate, and i is the annual inflation rate. For all cases, the only capital cost of main equipment is considered as CAPEX, and the replacement cost for fuel cells and lithium-ion batteries are included if applicable. In addition, the cost of fuel cells and lithium-ion batteries are predicted to decrease, while their lifetimes are expected to increase, as shown in Table 10.

Table 10. Lifetime and cost expectations for fuel cells and Li-ion batteries.

Item	Expected Lifetime	Increasing Rate of Lifetime for each Replacement	Decreasing Rate of Cost for each Replacement
PEMFC	6 year [86]	25% [87,88]	42% [87,88]
SOFC	5 year [89]	25% [87,88]	42% [87,88]
Li-ion battery	10–12 year ^{1,2} [90]	30% ² [91]	45% [92]

¹ 12 years for Cases 2–4 in which batteries are used for only cold start-ups, and 10 years for Case 5 in which batteries are used for dynamic load change. ² Assumed value based on a reference.

The OPEX is the sum of operation and maintenance (O&M) costs for each equipment and the fuel cost during the total lifetime of a ship. For Case 1, HFO fuel price is assumed at approximately \$ 405.0/t, which is the annual average value in 2019 for global 20 Ports [93]. In the other cases, the NH₃ fuel price is assumed to be about \$ 830/t [3], and the annual OPEX inflation rate and discount rate are assumed as 2% and 5%, respectively. The other auxiliary equipment installation cost and its O&M cost would be ignored based on the assumption that these costs are extremely small [86].

Additionally the cargo loss due to the increased volume of machinery for the proposed cases is not considered due to the difficulty of deciding the exact cargo cost. Table 11 shows the assumed equipment cost and O&M cost for the main equipment.

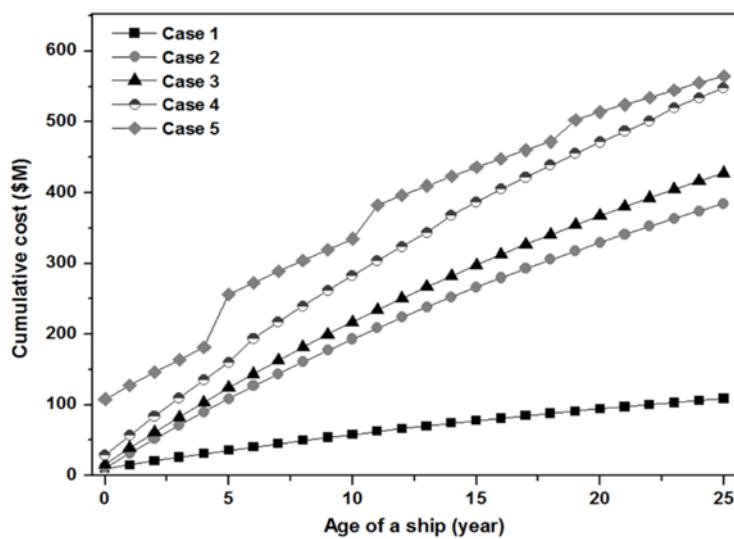
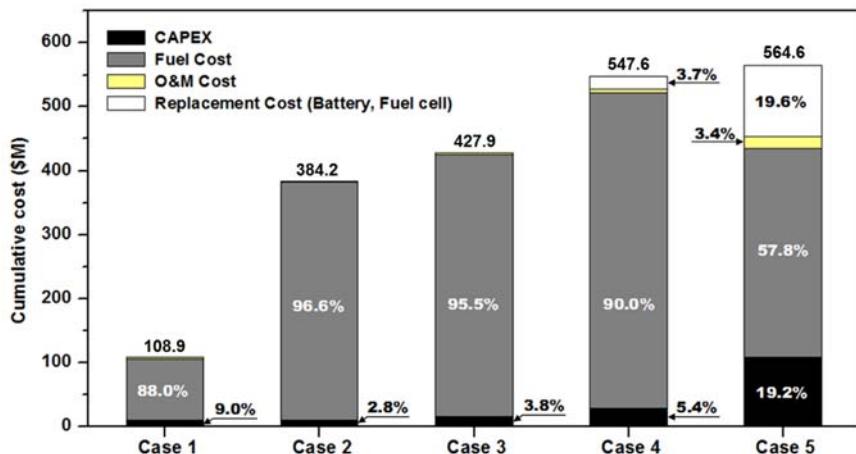
Table 11. Assumed equipment cost and operation and maintenance (O&M) cost for main equipment.

Equipment	CAPEX		OPEX	
	Equipment Cost	Reference	O&M Cost	Reference
M/E (HFO)	\$ 300/kW	[94]	\$ 5.2/kW/y	[95]
Genset (HFO)	\$ 350/kW	[95]	\$ 5.2/kW/y	[95]
M/E (NH ₃)	\$ 500/kW ¹	-	\$ 5.2/kW/y ²	-
Genset (NH ₃)	\$ 550/kW ¹	-	\$ 5.2/kW/y ²	-
PEMFC	\$ 1000/kW	[14]	1% of CAPEX	[88]
SOFC	\$ 5500/kW	[96]	1% of CAPEX ²	-
Li-ion Battery	\$ 500/kW ²	-	\$ 0.5/kW/y	[97]
Cracker (Engine) ³	\$ 670,000	[14]	1% of CAPEX	[14]
Cracker (PEMFC) ³	\$ 2,690,000	[14]	1% of CAPEX	[14]
Converter	\$ 200/kW	[98]	\$ 2/kW/y	[99]
VFD	\$ 200/kW	[98]	\$ 2/kW/y	[99]
Propulsion Motor	\$ 135/kW	[100]	1% of CAPEX	[14]
SCR	\$ 44/kW	[14,101]	3% of CAPEX	[102]
Scrubber	\$ 3,400,000	[103,104]	2% of CAPEX	[105]

¹ Assumed value including the additional cost for the NH₃ engine (non-corrosive material, special fuel system, etc.).

² Assumed value based on manufacturers' opinions. ³ Including burner and purifier.

Figure 11 shows the results of the cumulative cost for a ship with a 25-year lifespan, and Figure 12 shows the division of CAPEX, fuel cost, O&M cost, and replacement cost (battery, fuel cell). Among the proposed systems, the most economic system is Case 2, which is the M/E propulsion that is fueled by NH₃; however, its cumulative cost is about 3.5 times higher than Case 1. For Case 5, the CAPEX (19.2%) and the replacement cost (19.6%) have comparatively higher impacts, while the fuel cost (57.8%) is the lowest when compared to the others.

Figure 11. Cumulative cost for Cases 1–5 (NH_3 price = \$ 830/t).Figure 12. Division of the cumulative cost for Cases 1–5 (NH_3 price = \$ 830/t).

Even though the price of ammonia fuel is higher than that of conventional HFO, it is expected to decrease with stability because of improvements in the procurement of the ammonia supply chain. If the NH_3 price is decreasing same as the HFO price at \$ 405/t, the cumulative cost will be down 1.8 to 3.6 times than Case 1, depending on the system type, as shown in Table 12.

Table 12. Different cumulative cost for Cases 1–5, depending on the NH_3 price.

NH_3 Price	Cumulative Cost Comparison for Ship's Life Time				
	Case 1 (Base)	Case 2 (Times)	Case 3 (Times)	Case 4 (Times)	Case 5 (Times)
\$ 830/t	1.0	3.5	3.9	5.0	5.2
\$ 730/t	1.0	3.1	3.5	4.5	4.8
\$ 630/t	1.0	2.7	3.0	3.9	4.5
\$ 530/t	1.0	2.3	2.6	3.4	4.1
\$ 405/t	1.0	1.8	2.0	2.7	3.6

6. Conclusions

Ammonia is an intrinsically carbon-free fuel that produces zero CO₂ emissions when renewably sourced, and it is a clean fuel solution for engines and fuel cells. In this study, four possible propulsion systems that are all fueled by ammonia are suggested and compared with a focus on fuel consumption, and economic and environmental aspects. The results show that the ammonia-based ship would require more volume (1.6–2.3 times) and weight (1.4–1.6 times) than the conventional HFO-based ship, and it costs 3.5–5.2 times from the total lifecycle perspective. However, the NH₃-fueled ship could reduce GHG emissions by approximately 83.7–92.1%, which is dependent on the propulsion type and the fuel production method.

Among the proposed systems, Case 5, which is applied to the electric propulsion system powered by the SOFC and ESS, is the most eco-friendly system. However, it is the most expensive solution due to the high CAPEX than the others. Moreover, it requires more development in power density considering the high volume and weight. Alternatively, it is expected to compensate by integrating new technology, such as lightweight hull materials, the optimized space layout, etc. Furthermore, the cost-effectiveness is to be improved.

A number of additional challenges should also be solved to prove the feasibility of ammonia as a ship fuel. First of all, the main potential drawback is the safety issue (corrosion, toxicity, low flammability, etc.). However, ammonia has been handled as the liquefied gas cargo, a refrigerant, and an SCR reducing agent in ships, so the measures for these could enable the next step in enabling ammonia as a safe fuel.

On the regulatory side, some partial amendments to the section on the International Code of Safety for Ship Using Gases or Other Low-flashpoint Fuels (IGF Code) are required, and the International Gas Carrier Code (IGC Code) needs to allow for ammonia as a ship fuel. In addition, even though there are no classification rules for using ammonia as a fuel for ships, classification societies have already developed rules for ammonia carrier ships (ammonia tankers), refrigerated ships using ammonia, and thus these can be used as a basis for developing rules for ammonia as a fuel. In terms of the infrastructure, as ammonia has been already produced and transported in large quantities around the world, the industry's existing infrastructure could be used to realize bunker locations for ammonia-fueled ships in the future [106].

The economical and eco-friendly ships are of utmost importance for future sustainable development. Therefore, this new approach could be helpful in realizing carbon-free ships in the long-term perspective.

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